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CEE 577: Surface Water Quality Modeling

Lecture #13
BOD and Deoxygenation
(Chapra, L20)

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BOD Modeling

"L" is modelled as a simple 1st order decay: $\frac{dL}{dt} = -k_1 L$

Which leads to: $L = L_o e^{-k_1 t}$

And combining with: $BOD_t \equiv y_t = L_o - L_t$

We get: $BOD_t \equiv y_t = L_o (1 - e^{-k_1 t})$

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Temperature Effects

Temperature Dependence

- Chemist's Approach: Arrhenius Equation

$$\frac{d(\ln k)}{dT_a} = \frac{E_a}{RT_a^2}$$

$$k_{T_a} = k_{293^\circ K} e^{E_a(T_a - 293)/RT_a 293}$$

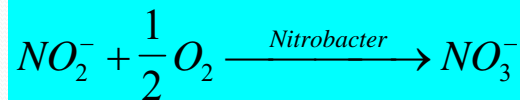
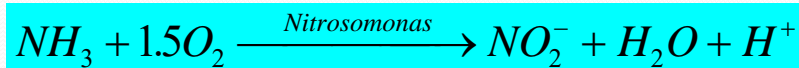
- Engineer's Approach:

$$k_T = k_{20^\circ C} \theta^{T - 20^\circ C}$$

Often we use:
 $\theta = 1.047$
 for CBOD

NBOD

Nitrogenous BOD (NBOD)



2 moles oxygen/1 mole of ammonia
 4.57 grams oxygen/gram ammonia-nitrogen

Like CBOD, the NBOD can be modelled as a simple 1st order decay:

$$\frac{dL^N}{dt} = -k_N L^N$$

NBOD cont.

- The model is then:

$$NBOD_t = L_o^N (1 - e^{-k_N t})$$

- where:
 - $L_o^N \equiv NBOD_u = 4.57(org - N + NH_3 - N)$
- Nitrifiers
 - very slow generation time (~1 day)
 - sensitive to low D.O.
- NBOD may be very important for non-nitrified, but otherwise highly treated waters

Typical Municipal WW Charact.

Parameter	Typical Wastewater Characteristics, mg/L except pH	U.S. EPA Discharge Standards, mg/L except pH	Typical Concentrations in Lakes or Streams, mg/L except pH
BOD ₅	150-300	30	2-10
Total Suspended Solids	150-300	30	2-20
COD	400-600	N/A	5-50
D.O.	0	4-5	4-Sat.
NH ₃ -N	15-40	*	<1
NO ₃	0	*	<1
pH	6-8	6-9	6-8

BOD Model

$$\frac{\partial L}{\partial t} = -U \frac{\partial L}{\partial x} - k_r L$$

Where the total removal rate is:

$$k_r = k_d + k_s$$

Decomposition rate in the stream
Settling rate

$$k_s = \frac{v_s}{H}$$

At steady state: $\frac{\partial L}{\partial t} = 0$

$$L = L_o e^{-k_r x/U}$$

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Estimating the k's

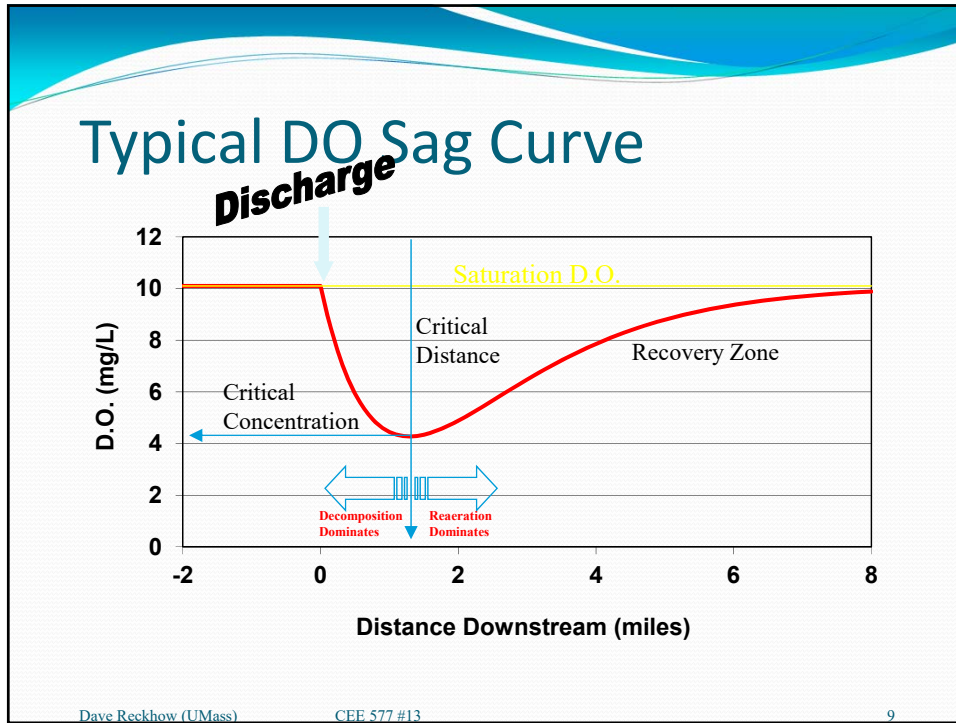
$$k_d = C \left(\frac{H}{8} \right)^{-0.434}, \quad 0 \leq H \leq 8 \text{ ft}$$

$$k_d = C, \quad H > 8 \text{ ft}$$

Where: C=0.2 for unstable bottoms
C=0.3 for rocky bottoms

$\theta \approx 1.047$

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Lecture #22
(Distributed Systems, time variable. Dye
Studies)

Chapra, Lio

Plug Flow (time variable)

- Simulating accidental spill, tracer studies

$$\frac{\partial c}{\partial t} = -U \frac{\partial c}{\partial x} - kc$$

- when a spill causes a concentration of c_0 at $x=0$ and $t=0$

$$c = c_0 e^{-kt^*}$$

Where: $t^* = x/U$

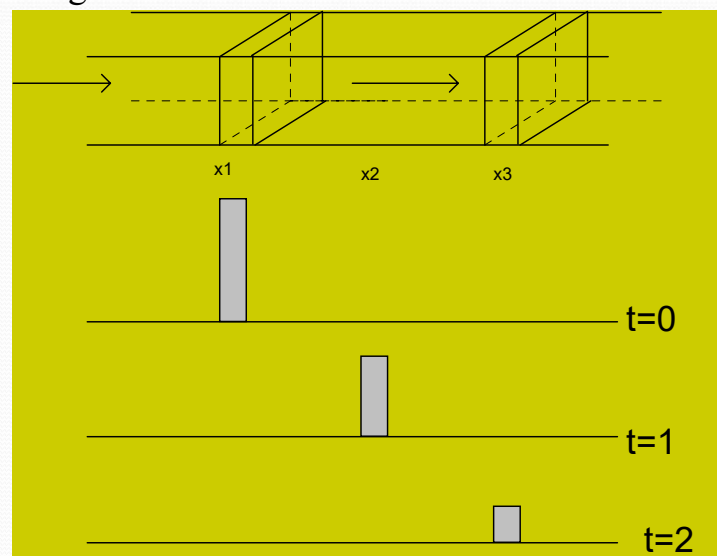
Refer to Example 10.1

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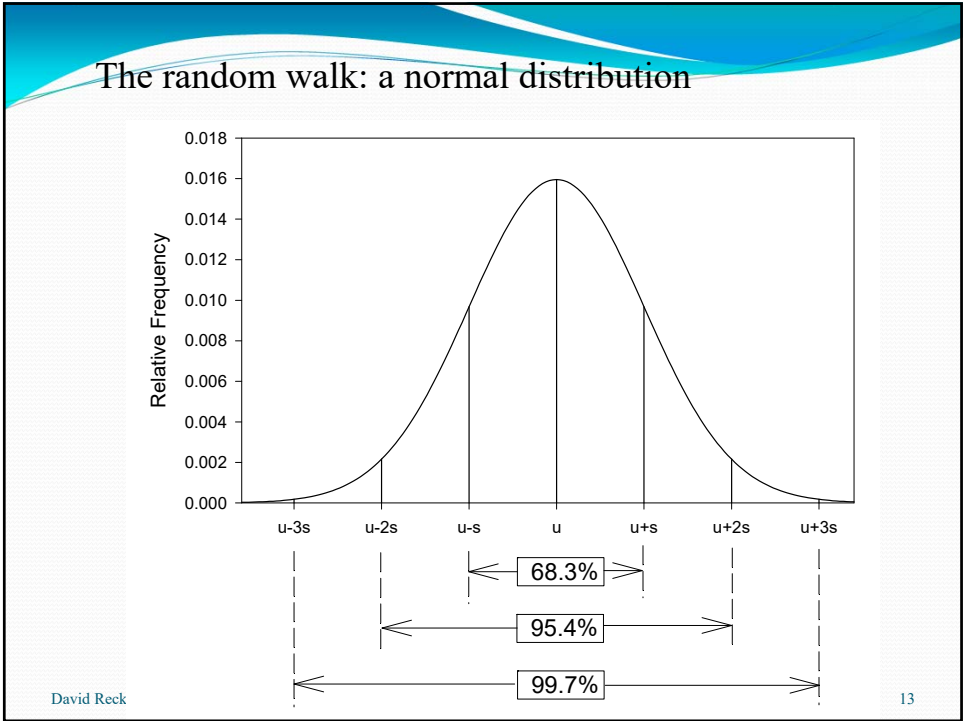
Moving vs. Fixed frame of reference



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Spill Models

- Dispersion and advection

$$c(x,t) = \frac{m_p}{2\sqrt{\pi Et}} e^{-\frac{(x-Ut)^2}{4Et}}$$

$\frac{m}{A_c}$

Equ# 10.24
in Chapra

- a normal distribution with:
 - $\bar{x} = Ut$
 - $\sigma = \sqrt{2Et}$

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Recall from our discussion on Longitudinal Dispersion (~Lecture #9)

- From Fischer et al., 1979

$$E = 0.011 \frac{U^2 B^2}{HU^*}$$

m^2s^{-1} → E m/s → U m → B m → H m → U^*
 Width (m) Mean depth (m)

Where the Shear Velocity is:

$$U^* = \sqrt{gHS}$$

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Empirical Method

- From Dye Study data
 - Method of moments

$$E_x = \frac{U^2}{2} \frac{\sigma_{td}^2 - \sigma_{tu}^2}{t_d - t_u}$$

Over length, at a single time

$$\sigma_l = \sqrt{2E_x t}$$

$$E_x = \frac{\sigma_l^2}{2t} = \frac{U^2}{2} \frac{\sigma_t^2}{t}$$

$$= \frac{U^2}{2} \frac{\Delta \sigma_t^2}{\Delta t}$$

Over time, at a specific location

- σ^2 = variance of the concentration-time curve
- t-bar = time of travel to the centroid of the curve
- The first moment about the origin gives:
 - where $t_{0.01}$ is the time at which concentration has decreases to 1% of the peak

$$\bar{t} = \frac{\int_0^{t_{0.01}} s t dt}{\int_0^{t_{0.01}} s dt}$$

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Empirical Method (cont.)

- And the 2nd moment about the centroid gives:

$$\sigma^2 = \frac{\int_0^{t_{0.01}} st^2 dt}{\int_0^{t_{0.01}} s dt} - (\bar{t})^2$$

- For discrete data these become:

$$\bar{t} = \frac{\sum st^{\Delta t}}{\sum s^{\Delta t}} = \frac{\sum st}{\sum s}$$

Compare to T&M equ 10.32

$$\sigma^2 = \frac{\sum st^{2\Delta t}}{\sum s^{\Delta t}} - (\bar{t})^2 = \frac{\sum st^2}{\sum s} - (\bar{t})^2$$

Compare to T&M equ 10.33

Dye Studies (cont.)

- Single point method
 - Use of peak concentration (c_p) and time to reach peak (t_p)

$$c_p = \frac{M}{2A\sqrt{\pi E_x}} (t_p)^{-0.5}$$

- plot c_p vs $(t_p)^{-0.5}$ to get a slope that is a function of E_x
- see sample problem 2.6 in T&M (pg. 78)

Homework #4

- Velocity
- dispersion coefficient

10 TECHNIQUES OF WATER-RESOURCES INVESTIGATIONS

TIME-OF-TRAVEL STUDY ON Millers River

SAMPLING SITE Millers Falls Paper Co. Bridge (RM 2.1)

Dye injected at Furley Bridge (RM 5.9) Time 9:55 Date 7/15/87

Amount injected 1 qt Type of dye _____ Conc. in % _____

Sampling section discharge 229 cfs; width _____; mean depth _____

Field Sampling and Analysis				Final Laboratory Analysis							
Sample No.	Sample Point	Sample Time	Fluorometer Readings				Fluorometer Readings				Dye Conc. (µg/L)
			1X	3X	10X	30X	1X	3X	10X	30X	
(1)	(2)	(3)	(4)	(5)	(6)	(7)	(8)	(9)	(10)	(11)	(12)
1		1030			24						
2		1045			24						
3		1100			24						
4		1115			27						
5		1130			40						
6		1145			39						
7		1200			41						
8		1215			28						
9		1230			29						
10		1245		13	43						
11		1300		29							
12		1315	20	60							
13		1330	32								
14		1345		18							
15		1400		16	53						
16		1415			42						
17		1430			28						
18+19		1445			26						
20		1500			24						

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USGS Guidelines: Input

- The USGS recommends the following volume or mass of Rhodamine WT-20% dye:

$$V_{dye} = 3.4 \times 10^{-4} \left(\frac{Q_m x}{U} \right)^{0.93} S_p$$

cfs → Q_m
 Miles downstream → x
 ft/sec → U
 Peak concentration desired at distance "x" → S_p
 Liters → V_{dye}
 lb → W_{dye}

$$W_{dye} = 2.62 V_{dye}$$

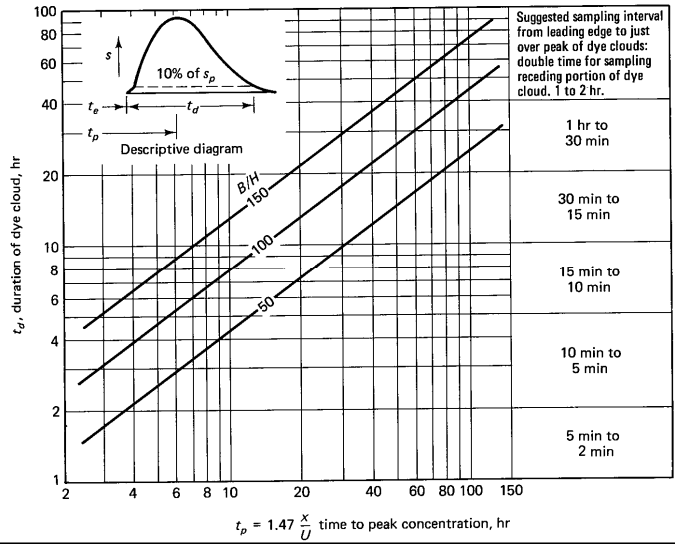
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USGS Guidelines: Sampling

- Duration of dye cloud as a function of travel time to peak, and average channel width-depth ratio (B/H).



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- [To next lecture](#)