

CEE 577: Surface Water Quality Modeling

Lecture #4
(mass balance, loadings & steady state
solutions)

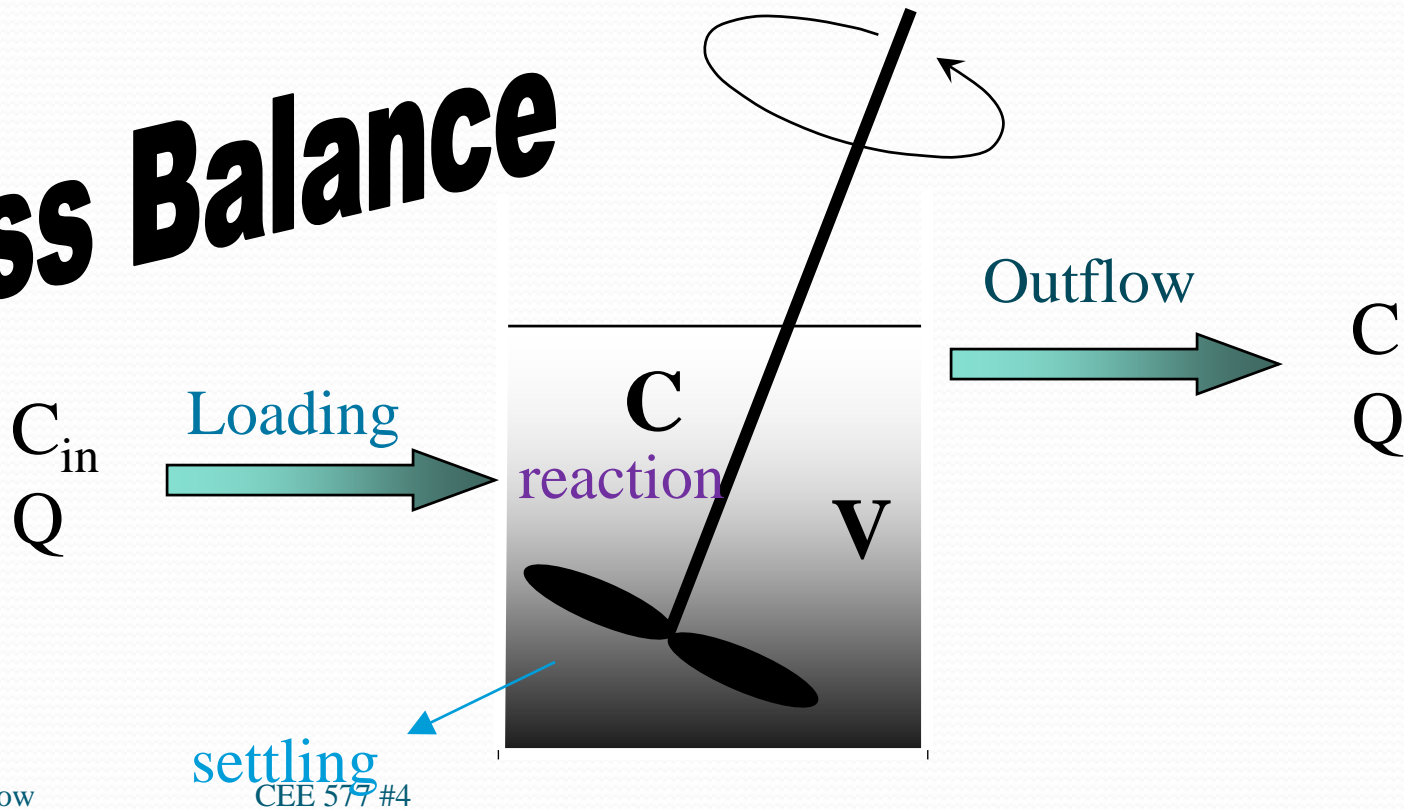
Chapra L3

Completely-mixed lake or CSTR

- Often useful to assume perfect mixing
 - same concentration throughout system

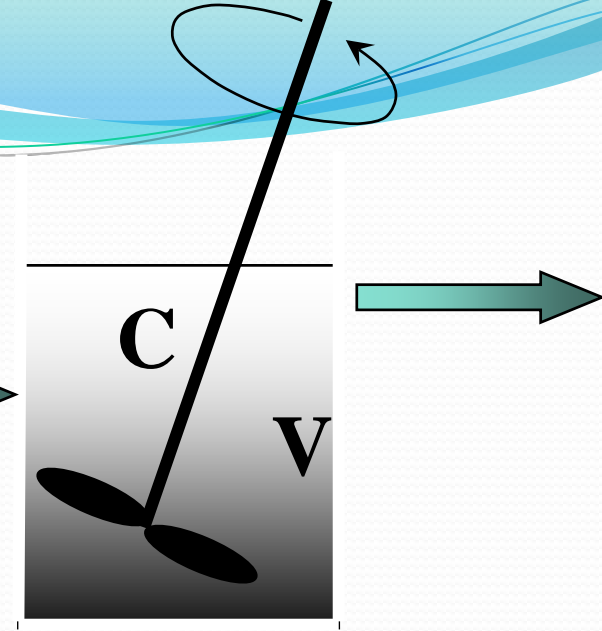
$$\text{Accumulation} = \text{loading} - \text{outflow} - \text{reaction} - \text{settling}$$

Mass Balance



Accumulation

$$\text{Accumulation} = \frac{\Delta M}{\Delta t}$$



and

$$c = \frac{M}{V}$$

$$M = Vc$$

$$\text{Accumulation} = \frac{\Delta Vc}{\Delta t}$$

And if volume is constant:

$$\text{Accumulation} = V \frac{\Delta c}{\Delta t} \rightarrow V \frac{dc}{dt}$$

Equals zero
at steady
state

Loading

$$Loading = W(t) = Qc_{in}(t)$$

- Point Sources
 - Municipal Wastewater
 - Industrial Wastewater
 - Tributaries
- Non-point sources
 - agricultural
 - silvicultural
 - atmospheric
 - urban & suburban runoff
 - groundwater

**Well defined origin
easily measured
more constant**

**Diffuse origin
more transient
often dependent on precipitation**

Reported Values Of Selected Waste Input Parameters In The United States

(Table 1.3 from Thomann & Mueller)

Variable	Units ^a	Municipal Influent ^b	CSO ^c	Urban Runoff ^d	Agriculture (lb/mi ² -d) ^e	Forest (lb/mi ² -d) ^e	Atmosphere (lb/mi ² -day) ^f
Average daily flow	gcd	125					
Total suspended solids	mg/L	300	410	610	2500	400	
CBOD5 ^g	mg/L	180	170	27	40	8	
CBODU ^g	mg/L	220	240				
NBOD ^g	mg/L	220	290				
Total nitrogen	mg-N/L	50	9	2.3	15	4	8.9-18.9
Total phosphorus	mg-P/L	10	3	0.5	1.0	0.3	0.13-1.3
Total coliforms	10 ⁶ /100 mL	30	6	0.3			
Cadmium	μg/L	1.2	10	13			0.015
Lead	μg/L	22	190	280			1.3
Chromium	μg/L	42	190	22			0.088
Copper	μg/L	159	460	110			
Zinc	μg/L	241	660	500			1.8
Total PCB	μg/L	0.9	0.3	-			0.002-0.02

Footnotes for T&M Table 1.3

- ^aUnits apply to municipal, CSO (combined sewer overflow), and urban runoff sources; gcd = gallons per capita per day.
- ^bThomann (1972); heavy metals and PCB, HydroQual (1982).
- ^cThomann (1972); total coli, Tetra Tech, (1977); heavy metals Di Toro et al. (1978): PCB. Hydroscience (1978).
- ^dTetra Tech (1977): heavy metals, Di Toro et al. (1978).
- ^eHydroscience (1976a).
- ^fNitrogen and phosphorus, Tetra Tech (1982): heavy metals and PC13, HydroQual (1982).
- ^gCBOD5 = 5 day carbonaceous biochemical oxygen demand (CBOD); CBODU = ultimate CBOD; NBOD = nitrogenous BOD.

Loading: Flow as a function of precipitation

- Non point sources are difficult to characterize
 - Empirical approach: export coefficients (see Table 3.1 in T&M)
 - Mechanistic approach: relate to meteorology, topology, etc.

• Flow: use the rational formula: $Q_R = cIA$

Runoff flow [L^3/T]

Runoff coefficient

Rainfall Intensity [L/T]

Drainage Area [L^2]

0.1-0.3 for rural areas (1 person/acre)
0.7-0.9 for heavy commercial areas

Note:

1 acre-in/hr \approx 1 cfs

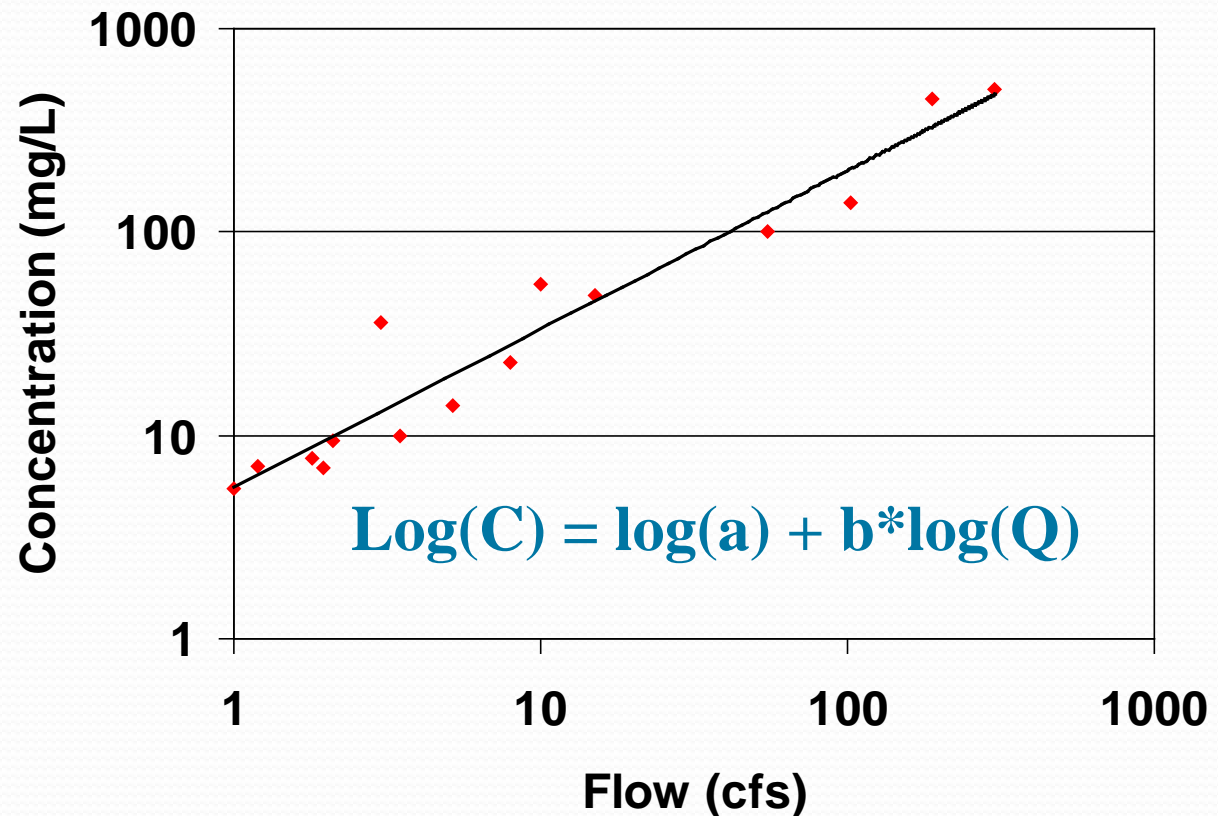
Runoff: Contrasting approaches

- Lumped model
 - Empirical
 - Built on a single rainfall intensity from rain gage data
- Distributed model
 - Mechanistic
 - Built on radar data for rainfall
 - Spatial & temporal resolution
 - Combine with overland flow models
 - Many computer codes
 - CASC2D, CUHP, CUHP/SWMM, DR₃M, HEC-1, HSPF, PSRM, SWMM, TR₂₀

Loading: conc. as a function of flow

- It is common for pollutant concentrations from uncontrolled sources (e.g. tributaries) to be correlated with flow

- establish a log-log relationship
- $c = aQ^b$



Loading Example: #3.1 from T&M

- Data: Runoff from 100 mi² of agricultural lands drains to a point in a river where a city of 100,000 people is located. The city has a land area of 10 mi² and its sanitary sewers are separated from its storm drains. A sewage treatment plant discharges to the river immediately downstream of the city. The area receives an annual rainfall of 30 in. of which 30% runs off the agricultural lands and 50% drains off the more impervious city area.
- Problem: Using the loading data from Table 1.3 and the residual fractions cited in the table below, compare the contributions of the atmospheric, agricultural and urban sources to annual average values of flow, CBOD₅, total coliform bacteria, and lead in the river. Neglect any decay mechanisms for all parameters.

Item	(at)	(ag)	(ur)	Wastewater Treatment Plant	
	Atmospheric	Agricultural	Urban Runoff	Influent	Resid. Fract.
Flow		30% precip.	50% precip.	125 gpd	1.00
CBOD ₅		40 lb/mi ² -d	27 mg/L	180 mg/L	0.15
Total coliform		100/100 mL	3x10 ⁵ /100mL	3x10 ⁶ /100mL	0.0001
Lead	1.3 lb/mi ² -d		280 µg/L	22 µg/L	0.05

Solution to loading problem

- Flow contributions

$$\begin{aligned} Q(ag) &= 100mi^2 (30in / yr) 0.3 \left(\frac{5280ft}{mi} \right)^2 \frac{1ft}{12in} \frac{1yr}{365d} \frac{1d}{86,400s} \\ &= 66.3cfs \end{aligned}$$

$$\begin{aligned} Q(ur) &= 10mi^2 (30in / yr) 0.5 \left(\frac{5280ft}{mi} \right)^2 \frac{1ft}{12in} \frac{1yr}{365d} \frac{1d}{86,400s} \\ &= 11.1cfs \end{aligned}$$

$$\begin{aligned} Q(wwtp) &= 100,000cap \frac{125gal}{cap-d} \frac{1MG}{10^6gal} \\ &= 12.5MGD \left(\frac{1.548cfs}{MGD} \right) \\ &= 19.4cfs \end{aligned}$$

Solution to loading problem (cont.)

- CBOD₅ loading

$$\begin{aligned}W(ag) &= 100mi^2 \left(40 \frac{lb}{mi^2 d} \right) \\ &= 4000 \frac{lb}{d}\end{aligned}$$

$$\begin{aligned}W(ur) &= 11.1cfs(27mg/L)5.4 \frac{lb/d}{cfs \cdot mg/L} \\ &= 1620 \frac{lb}{d}\end{aligned}$$

$$\begin{aligned}W(wwtp) &= 12.5MGD(180mg/L)0.15 \left(\frac{8.34lb/d}{MGD \cdot mg/L} \right) \\ &= 2810 \frac{lb}{d}\end{aligned}$$

Solution to loading problem (cont.)

- Lead loading

$$W(atm) = 100mi^2 \left(1.3 \frac{lb}{mi^2 d} \right) 0.1$$
$$= 13 \frac{lb}{d}$$

$$W(ur) = 11.1cfs(280\mu g / L)5.4 \frac{lb / d}{cfs - mg / L} \left(\frac{10^{-3} mg}{\mu g} \right)$$
$$= 16.8 \frac{lb}{d}$$

$$W(wwtp) = 12.5MGD(22\mu g / L)0.05 \left(\frac{8.34lb / d}{MGD * mg / L} \right) \frac{10^{-3} mg}{\mu g}$$
$$= 0.11 \frac{lb}{d}$$

Other Terms in the Mass Balance

- Outflow

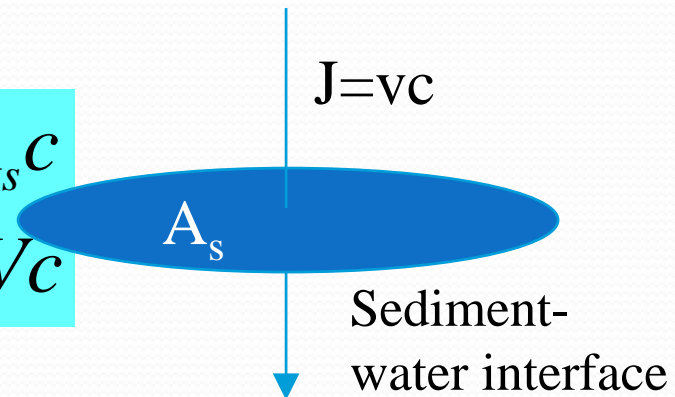
$$\text{Outflow} = Qc$$

- Reaction

$$\text{Reaction} = kM = kVc$$

- Settling

$$\begin{aligned}\text{Settling} &= vA_s c \\ &= k_s Vc\end{aligned}$$



Since:

$$k_s = v/H$$

$$V = A_s H$$

Combining all terms:

$$V \frac{dc}{dt} = W(t) - Qc - kVc - vA_s c$$

- Dependent variable: c
- Independent variable: t
- Forcing function: $W(t)$, the way in which the external world “forces” the system
- Parameters: V, Q, k, v, A_s

Steady State Case

- Mass Balance

$$V \frac{dc}{dt} = 0 = W(t) - Qc - kVc - vA_s c$$

- Solution

$$c = \frac{W}{Q + kV + vA_s}$$

or

$$c = \frac{W}{a}$$

W

- Assimilation factor

- Where

$$a = Q + kV + vA_s$$

- The assimilation or “cleansing” factor

Steady State Example

#3.1 from Chapra (pg.52)

A lake has the following characteristics:

$$\begin{aligned} \text{Volume} &= 50,000 \text{ m}^3 \\ \text{Mean Depth} &= 2 \text{ m} \\ \text{Inflow} &= \text{Outflow} = 7500 \text{ m}^3 \text{d}^{-1} \\ \text{Temperature} &= 25^\circ \text{C} \end{aligned}$$

The lake receives the input of a pollutant from three sources: a factory discharge of 50 kg d^{-1} , a flux from the atmosphere of $0.6 \text{ g m}^{-2} \text{ d}^{-1}$, and the inflow stream that has a concentration of 10 mg/L . If the pollutant decays at the rate of $0.25/\text{d}$ at 20°C (note: $\Theta=1.05$).

- compute the assimilation factor
- steady state concentration
- show breakdown for each term

Example 3.1: Solution

First correct the decay rate for temperature

$$\begin{aligned}k &= 0.25\theta^{25-20} = 0.25(1.05)^{25-20} \\ &= 0.319d^{-1}\end{aligned}$$

Now the assimilation factor

$$\begin{aligned}a &= Q + kV \\ &= 7500 + 0.319(50,000) \\ &= 23,454m^3d^{-1}\end{aligned}$$

Example 3.1: Solution (cont.)

The surface area of the lake is:

$$A_s = \frac{V}{H} = \frac{50,000}{2} = 25,000m^2$$

The atmospheric and inflow load is then:

$$W_{atmosphere} = JA_s = 0.6(25,000) = 15,000g / d$$

$$W_{inflow} = 7500(10) = 75,000g / d$$

Combining all loads:

$$\begin{aligned} W &= W_{factory} + W_{atmosphere} + W_{inflow} \\ &= 50,000 + 15,000 + 75,000 \\ &= 140,000g / d \end{aligned}$$

Example 3.1: Solution (cont.)

And finally, the concentration:

$$\begin{aligned}c &= \frac{W}{a} \\ &= \frac{140,000 \text{ g} / d}{23,454 \text{ m}^3 / d} \\ &= 5.97 \text{ mg} / L\end{aligned}$$

Transfer function & residence time

$$c = \frac{W}{Q + kV + vA_s}$$

$$= \frac{Qc_{in}}{Q + kV + vA_s}$$

$$\frac{c}{c_{in}} = \beta \equiv \frac{Q}{Q + kV + vA_s}$$

Transfer function

$$\tau_E = \frac{E}{dE/dt}$$

generic

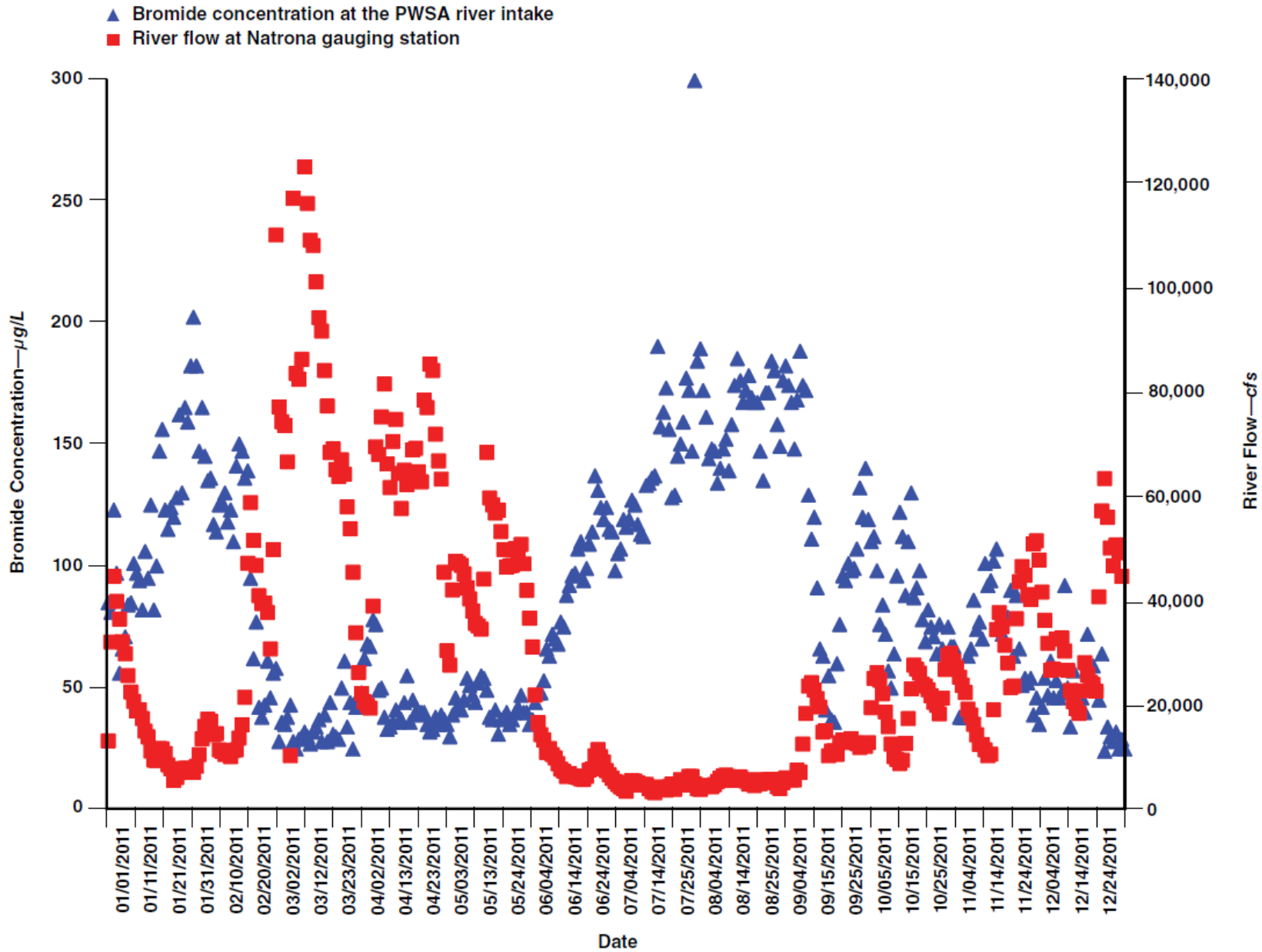
Residence
times

$$\tau_w = \frac{V}{Q} \text{ water}$$

$$\tau_c = \frac{Vc}{Qc + kVc + vA_s c} = \frac{V}{Q + kV + vA_s}$$

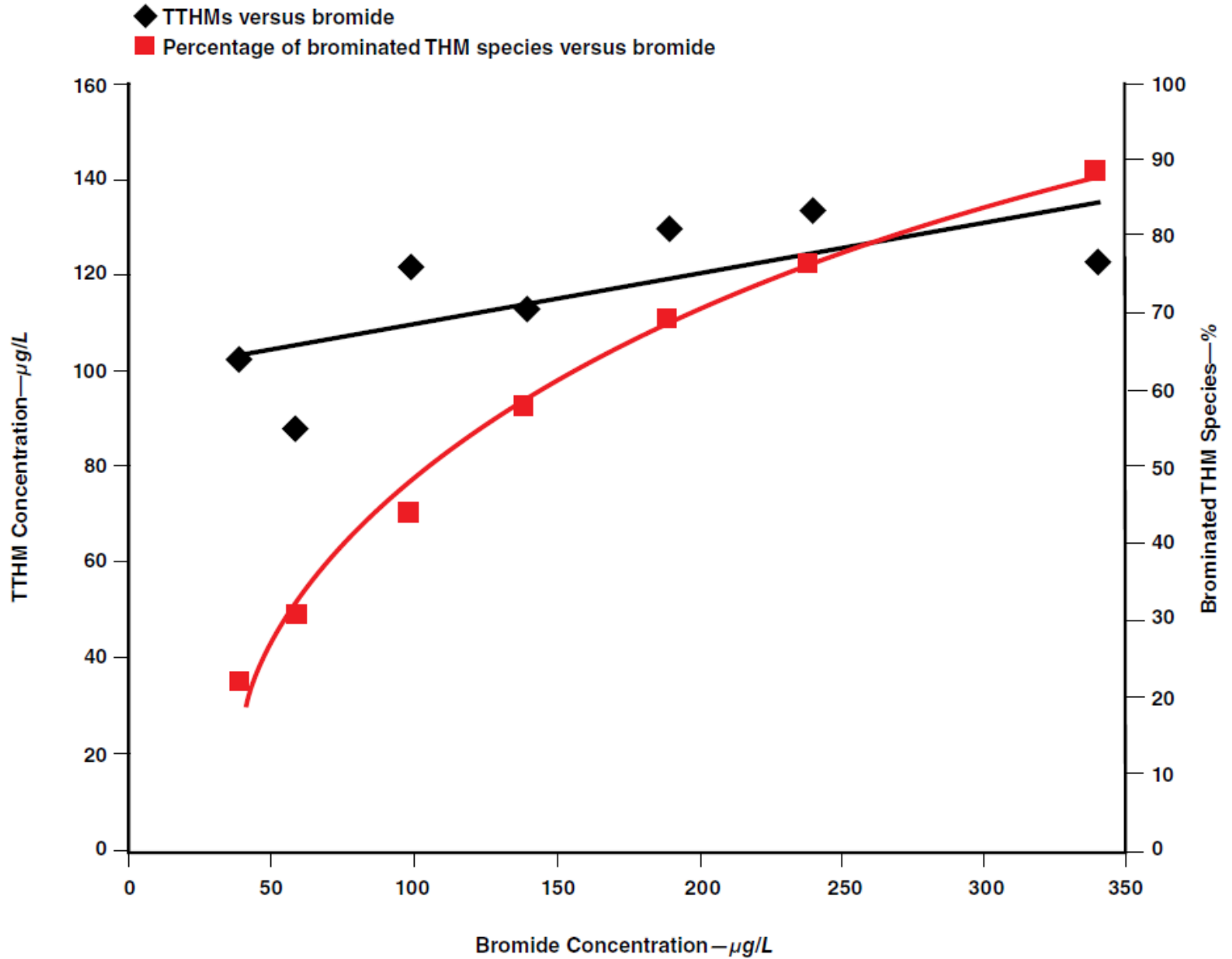
contaminant

FIGURE 3 Bromide concentration and river flow



● P.

FIGURE 2 TTHM formation potential study—effect of experimental addition of bromide



TTHMs—total trihalomethanes

FIGURE 4 The Allegheny River system

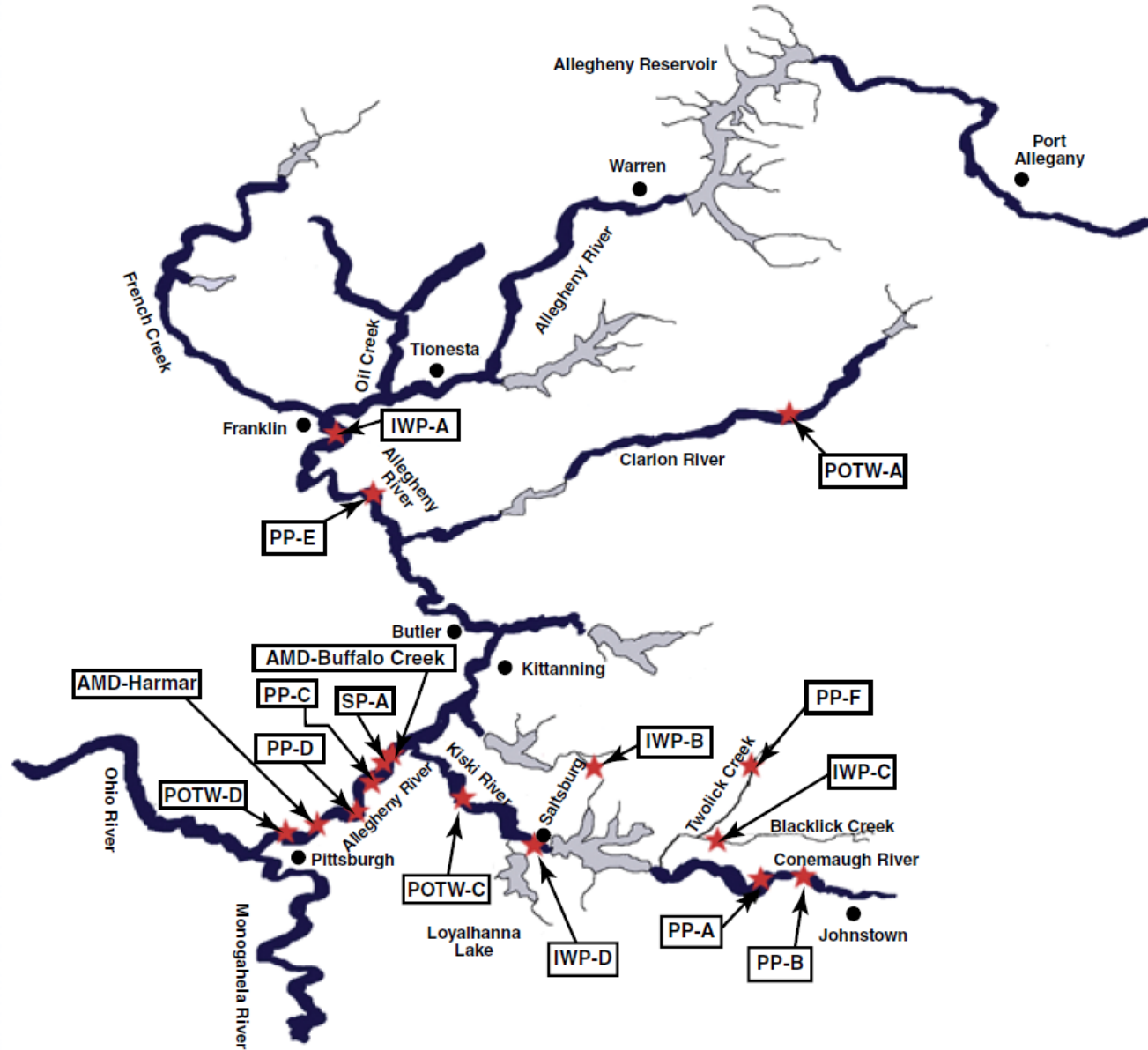
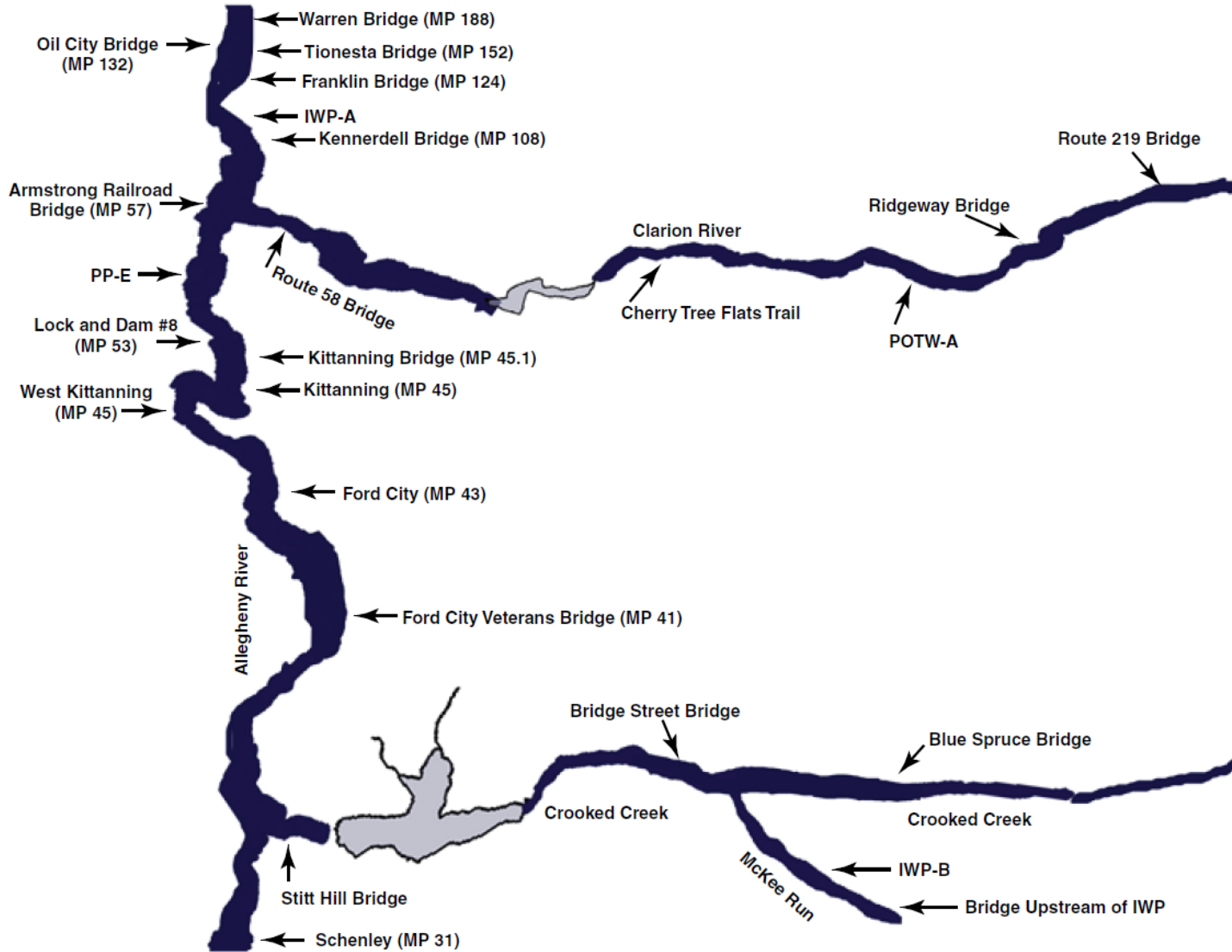


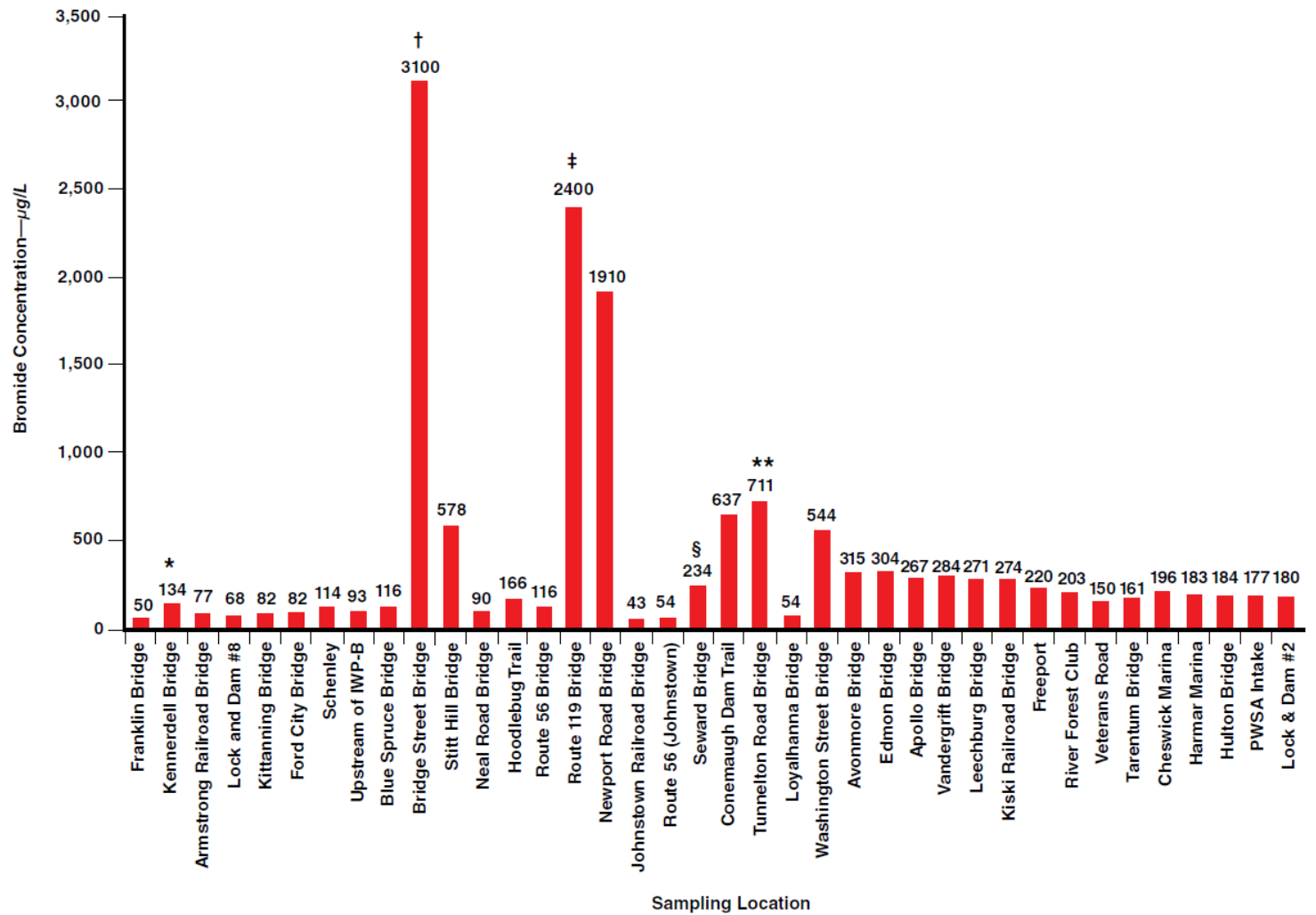
FIGURE 5 The Upper Allegheny River system



IWP—industrial waste plant, MP—mile point, POTW—publicly owned treatment works, PP—power plant

Map not to scale

FIGURE 7 Results of PWSA bromide sampling in July 2011



IWP-B—industrial waste plant B, PWSA—Pittsburgh Water and Sewer Authority

* Downstream of industrial waste plant A

† Downstream of industrial waste plant B

‡ Downstream of industrial waste plant C

§ Downstream of industrial waste plant A and B

Bromide in PA

Kelly D. Good and Jeanne M. VanBriesen, 2016
 “Current and Potential Future Bromide Loads from Coal-Fired Power Plants in the Allegheny River Basin and Their Effects on Downstream Concentrations”, *ES&T* 50, 9078

LEGEND

- USGS streamflow gage
- USGS streamflow gage used in model
- ▲ Power plant with wet FGD
- Br sampling site used in model (see Table 1)
 - 1 – PWSA
 - 2 – 3RQ
- Model site

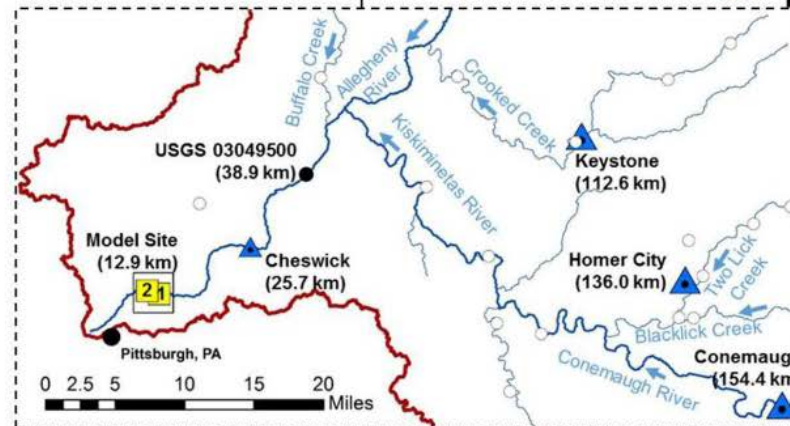
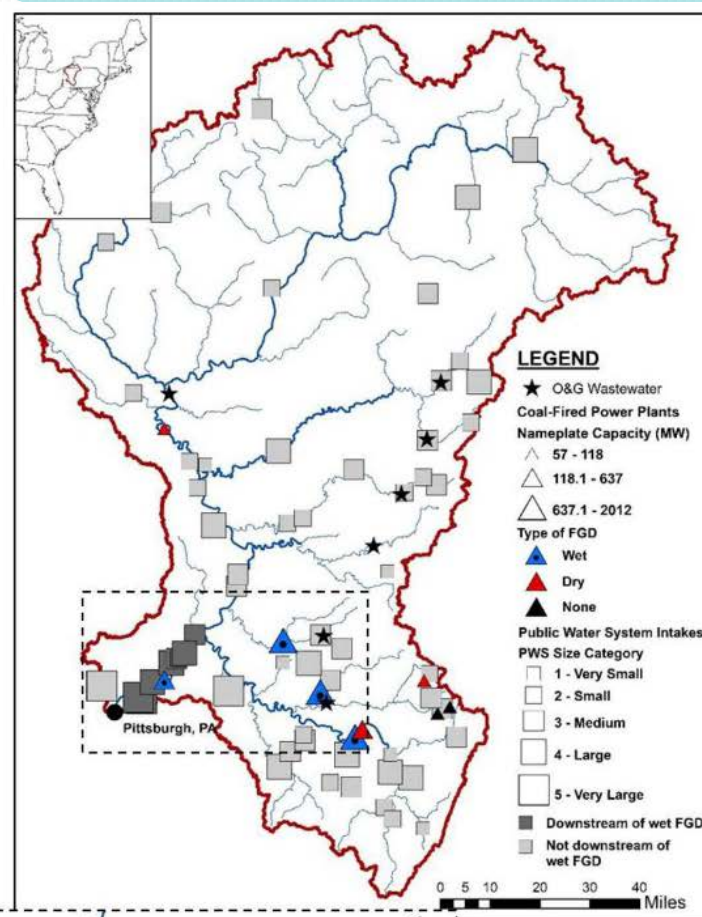


Figure 1. Map of the Allegheny River Basin showing coal-fired power plants and public drinking water systems. Inset map shows wet FGD power plants (blue triangles), USGS streamflow gage used in the model (black circle), sampling sites for bromide (yellow squares), and the model site at river kilometer (RKM) 12.9. Distances provided are RKM measured from the confluence in Pittsburgh, PA.

Calculation for estimated Baseline wet FGD bromide load (kg/day)

$$\left(\begin{array}{c} \text{Estimated} \\ \text{Baseline} \\ \text{wet FGD Br load,} \\ \text{kg/day} \end{array} \right) = \left(\begin{array}{c} \text{Br capture in} \\ \text{wet FGD,} \\ \% \end{array} \right) \times \left(\begin{array}{c} \text{Wet-FGD associated} \\ \text{coal consumption,} \\ \text{dry basis, kg/day} \end{array} \right) \times \left(\frac{\text{million kg}}{10^6 \text{ kg}} \right) \times \left(\begin{array}{c} \text{Br content} \\ \text{dry coal, ppm} \end{array} \right)$$

Where:

$$\left(\begin{array}{c} \text{Wet-FGD associated} \\ \text{coal consumption,} \\ \text{dry basis, kg/day} \end{array} \right) = \left(\begin{array}{c} \text{Wet-FGD associated} \\ \text{coal consumption,} \\ \text{as received,} \\ \text{tons/month} \end{array} \right) \times \left(\frac{2000 \text{ lb}}{\text{ton}} \right) \times \left(\frac{\text{kg}}{2.2 \text{ lb}} \right) \times \left(\frac{\text{month}}{\text{days}} \right) \times \left(\frac{1}{1 - \left(\frac{\text{moisture}}{\text{content, \%}} \right)} \right)$$

$$\left(\begin{array}{c} \text{Br content} \\ \text{dry coal, ppm} \end{array} \right) = \left(\begin{array}{c} \text{Br/Cl content} \\ \text{in coal} \end{array} \right) \times \left(\begin{array}{c} \text{Cl content} \\ \text{dry coal, ppm} \end{array} \right)$$

Calculation for estimated Br Addition wet FGD bromide load (kg/day)

Same as above, except for Br added for Hg control, as shown below.

$$\left(\begin{array}{c} \text{Estimated} \\ \text{Br Addition} \\ \text{wet FGD Br load,} \\ \text{kg/day} \end{array} \right) = \left(\begin{array}{c} \text{Br capture} \\ \text{in wet FGD,} \\ \% \end{array} \right) \times \left(\begin{array}{c} \text{Wet-FGD associated} \\ \text{coal consumption,} \\ \text{dry basis, kg/day} \end{array} \right) \times \left(\frac{\text{million kg}}{10^6 \text{ kg}} \right) \times \left[\left(\begin{array}{c} \text{Br content} \\ \text{dry coal, ppm} \end{array} \right) + \left(\begin{array}{c} \text{Br added for} \\ \text{Hg control,} \\ \text{ppm in} \\ \text{dry coal} \end{array} \right) \right]$$

Calculation for estimated oil and gas (O&G) wastewater bromide load (kg/day)

$$\left(\begin{array}{c} \text{Estimated} \\ \text{O\&G wastewater} \\ \text{Br load,} \\ \text{kg/day} \end{array} \right) = \left(\begin{array}{c} \text{POTW Br load,} \\ \text{kg/day} \end{array} \right) + \left(\begin{array}{c} \text{CWT Br load,} \\ \text{kg/day} \end{array} \right)$$

Where:

$$\left(\begin{array}{c} \text{POTW Br load,} \\ \text{kg/day} \end{array} \right) = \left(\begin{array}{c} \text{POTW Br load,} \\ \text{lb/day} \end{array} \right) \times \left(\frac{\text{kg}}{2.2 \text{ lb}} \right)$$

$$\left(\begin{array}{c} \text{CWT Br load,} \\ \text{kg/day} \end{array} \right) = \left(\begin{array}{c} \text{Maximum} \\ \text{daily flow,} \\ \text{mgd} \end{array} \right) \times \left(\frac{10^6 \text{ gal}}{\text{MG}} \right) \times \left(\frac{3.7854 \text{ L}}{\text{gal}} \right) \times \left(\begin{array}{c} \text{Average TDS} \\ \text{concentration,} \\ \text{mg/L} \end{array} \right) \times \left(\begin{array}{c} \text{Median} \\ \text{Br/TDS ratio} \end{array} \right) \times \left(\frac{\text{kg}}{10^6 \text{ mg}} \right)$$

Calculation for estimated nonpoint bromide load (kg/day)

$$\left(\begin{array}{c} \text{Estimated} \\ \text{nonpoint} \\ \text{Br load,} \\ \text{kg/day} \end{array} \right) = \left(\begin{array}{c} \text{Nonpoint Br} \\ \text{concentration,} \\ \mu\text{g/L} \end{array} \right) \times \left(\begin{array}{c} \text{Streamflow,} \\ \text{m}^3/\text{sec} \end{array} \right) \times \left(\frac{1000 \text{ L}}{\text{m}^3} \right) \times \left(\frac{\text{kg}}{10^9 \mu\text{g}} \right) \times \left(\frac{86400 \text{ sec}}{\text{day}} \right)$$

Where nonpoint Br concentration is assumed to be 22 µg/L at the Model Site, as described in the paper.

- To next lecture