Updated: 16 October 2019   Print version

CEE 370
Environmental Engineering
Principles

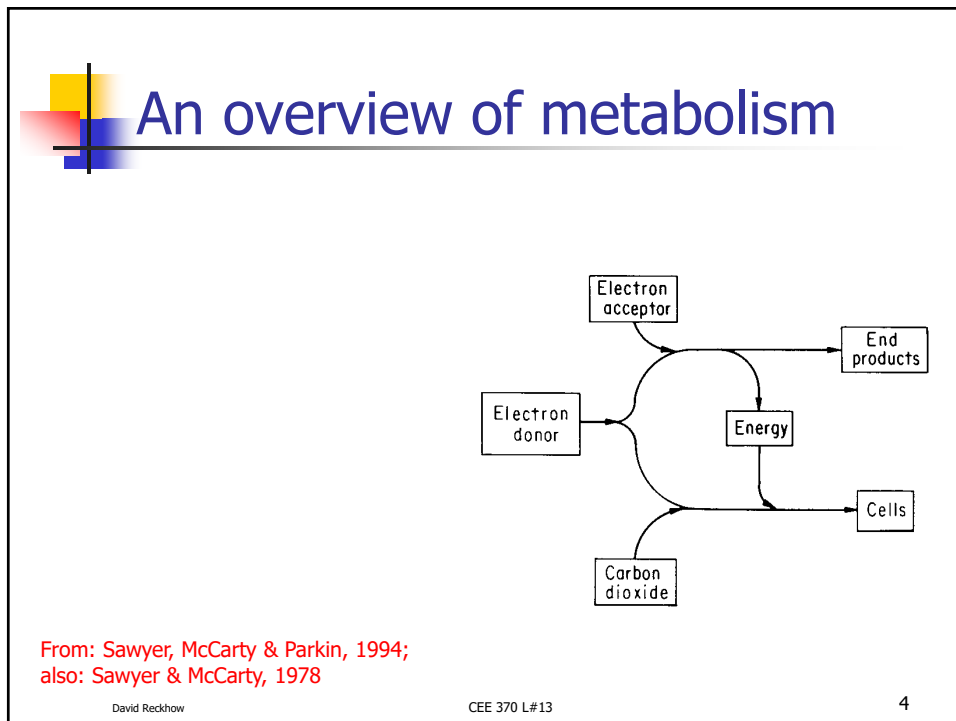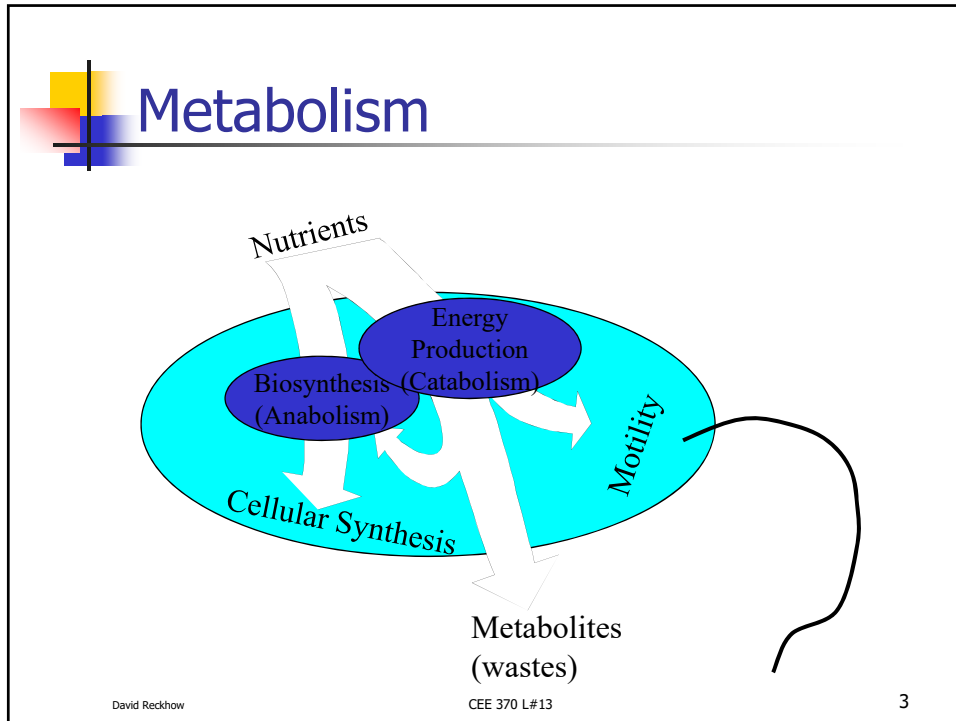Lecture #13
Environmental Biology II
Metabolism
Reading: Mihelcic & Zimmerman, Chapter 5

Davis & Masten, Chapter 3

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Environmental Microbiology

- Types of Microorganisms
  - Bacteria
  - Viruses
  - Protozoa
  - Rotifers
  - Fungi
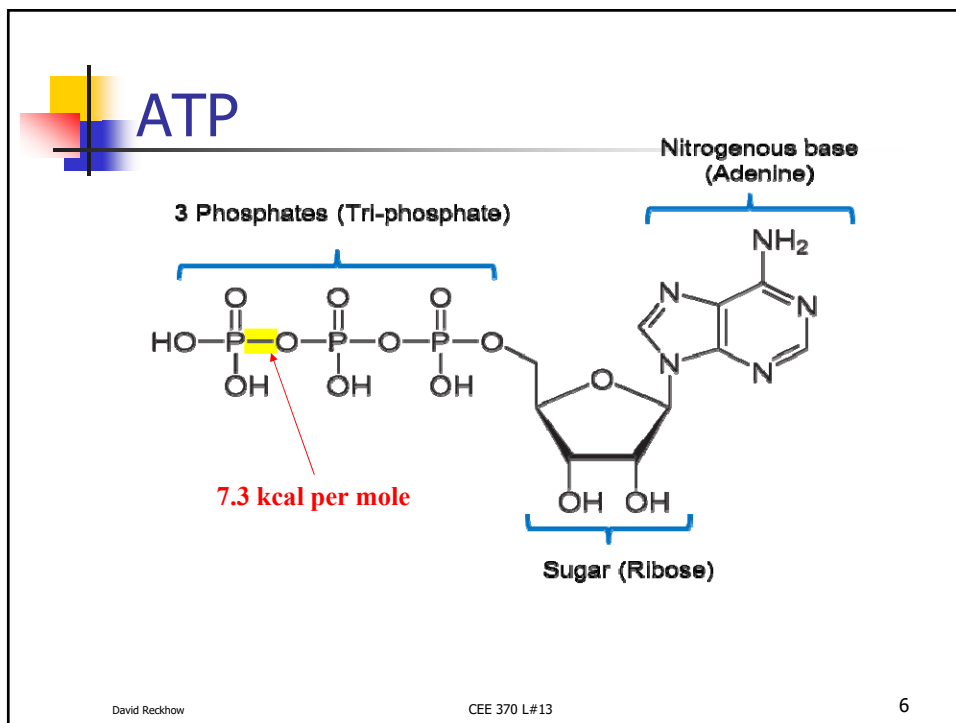- Metabolism
- Microbial Disease
- Microbial Growth

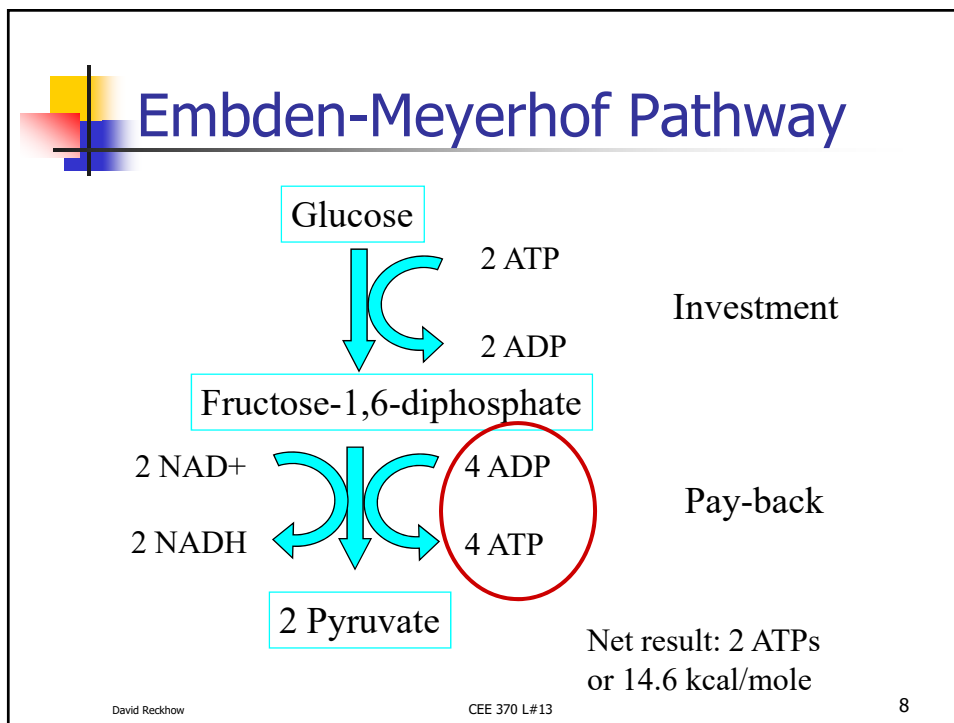David Reckhow   CEE 370 L#13   2

Metabolism

Nutrients

Energy
Production
(Catabolism)

Biosynthesis
(Anabolism)

Motility

Cellular Synthesis

Metabolites
(wastes)

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An overview of metabolism

Electron
acceptor

End
products

Electron
donor

Energy

Cells

Carbon
dioxide

From: Sawyer, McCarty & Parkin, 1994;
also: Sawyer & McCarty, 1978

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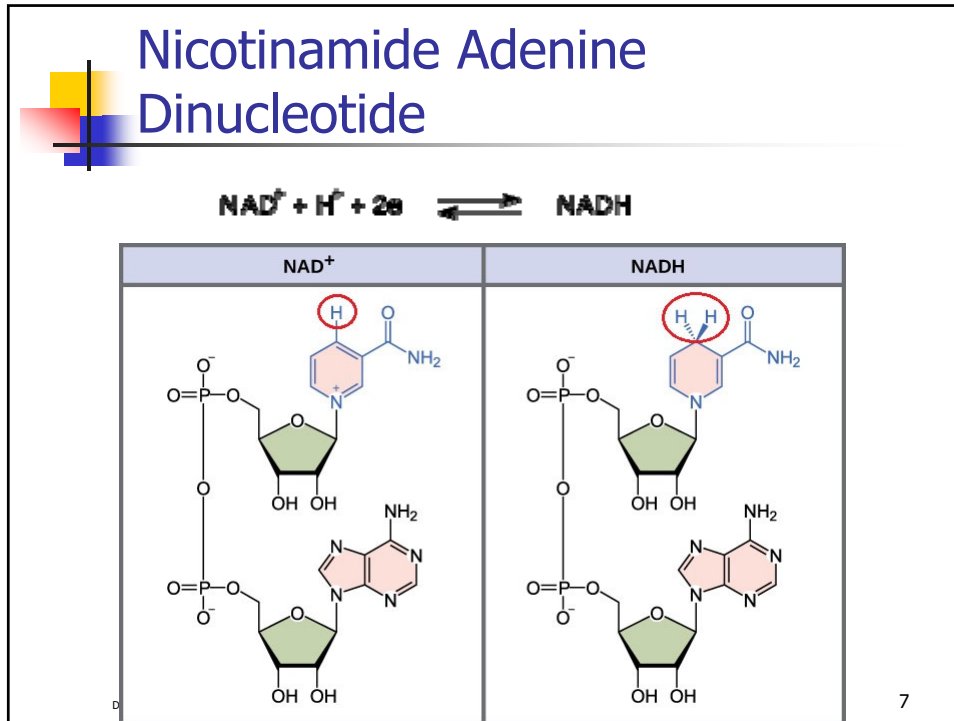
Energy

➢Source
  ➢Light
  ➢Chemicals (e.g., glucose)
➢Storage
  ➢ATP
  ➢NAD+
➢Advantages of oxygen as a terminal electron acceptor
  ➢aerobic
  ➢anaerobic
  ➢facultative
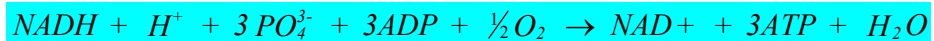
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ATP

Nitrogenous base
(Adenine)

3 Phosphates (Tri-phosphate)

NH₂

HO—P=O—P—O—P—O

OH   OH   OH

7.3 kcal per mole

OH OH

Sugar (Ribose)

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Nicotinamide Adenine Dinucleotide

$$NAD^+ + H^+ + 2e \rightleftharpoons NADH$$

NAD$^+$	NADH

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Embden-Meyerhof Pathway

Glucose

2 ATP

Investment

2 ADP

Fructose-1,6-diphosphate

2 NAD+   4 ADP

Pay-back

2 NADH   4 ATP

2 Pyruvate

Net result: 2 ATPs
or 14.6 kcal/mole

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Advantages of Aerobic Systems

If we have aerobic metabolism, rather than fermentation, energy from NADH may be harvested.

$$NADH + H^+ + 3\,PO_4^{3-} + 3ADP + \tfrac{1}{2}O_2 \rightarrow NAD+ + 3ATP + H_2O$$

This gives us 6 more ATPs. Then the pyruvate may be further oxidized to carbon dioxide and water, producing 30 more ATPs. The final tally is 38 ATPs or 277 kcal/mole of glucose.
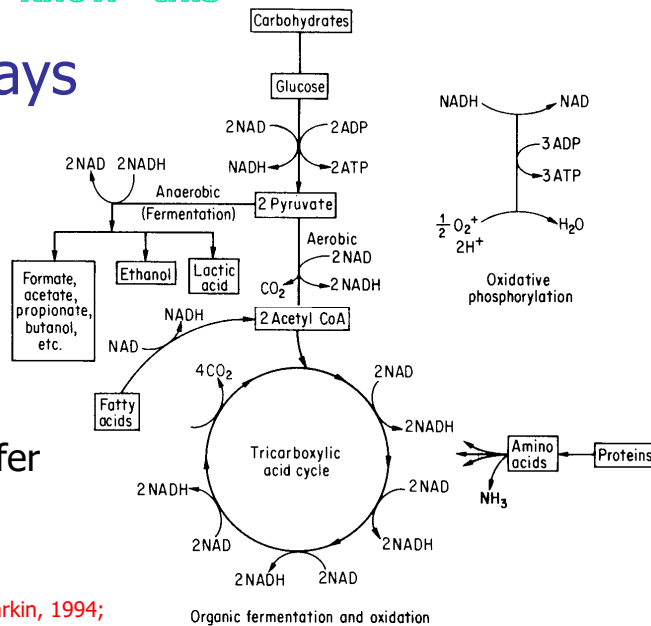
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Don't need to "know" this

Pathways

- Generalized view of both aerobic and fermentative pathways
- Also showing energy transfer
  - ATP
  - NAD

From: Sawyer, McCarty & Parkin, 1994; also: Sawyer & McCarty, 1978

Organic fermentation and oxidation

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Metabolic Classification

✿ Carbon Source
- ✿ Heterotrophic: other organic matter
- ✿ Autotrophic: inorganic carbon (CO_2)

✿ Energy Source (electron donor)
- ✿ Chemosynthetic: chemical oxidation
- ✿ Photosynthetic: light energy

✿ Terminal Electron Acceptor
- ✿ Aerobic: oxygen
- ✿ Anaerobic: nitrate, sulfate
- ✿ Fermentative: organic compounds

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Energy Flow

$$CO_2 + H_2O \xrightarrow[\text{Chlorophyll}]{\text{Light Energy } (\Delta)} C(H_2O) + O_2$$

(a) Photosynthesis

- ■ Storage of Energy
  - ■ Photosynthesis
- ■ Release of Energy
  - ■ Respiration

$$O_2 + C(H_2O) \longrightarrow CO_2 + H_2O + \Delta \text{ Energy}$$

(b) Respiration

- ■ Energy transfers by organisms are inherently inefficient
  - ■ 5-50% capture

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Aerobic Respiration

$$O_2 + C(H_2O) \longrightarrow CO_2 + H_2O + \Delta \text{ Energy}$$

- A Redox reaction
  (b) Respiration
  - Oxidation of Carbon
    $$C(H_2O) + H_2O \rightarrow CO_2 + 4H^+ + 4e^-$$
  - Reduction of oxygen or some other terminal electron acceptor
    $$O_2 + 4H^+ + 4e^- \rightarrow 2H_2O$$

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Other TEA: Anaerobic Respiration

- Nitrate
  $$C(H_2O) + NO_3^- \rightarrow N_2 + CO_2 + HCO_3^- + H_2O$$
- Manganese
  $$C(H_2O) + Mn^{+4} \rightarrow Mn^{+2} + CO_2 + H_2O$$
- Iron
  $$C(H_2O) + Fe^{+3} \rightarrow Fe^{+2} + CO_2 + H_2O$$
- Sulfate
  $$C(H_2O) + SO_4^{-2} \rightarrow H_2S + CO_2 + H_2O$$
- Fermentation
  $$C(H_2O) \rightarrow CH_4 + CO_2$$
  methanogenesis

Ecological Redox Sequence

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Terminal Electron Acceptors

- Contribution to the oxidation of organic matter
  - Bottom waters of Onondaga Lake, NY
  - (Effler, 1997)

Pie chart: Iron Reduction 1%, Methanogenesis 23%, Aerobic 39%, Nitrate Reduction 10%, Sulfate Reduction 27%

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Energetics

- Principles of Gibbs Free Energy and Energy Balance can be applied to microbial growth

From: Sawyer, McCarty & Parkin, 1994; also: Sawyer & McCarty, 1978

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Reaction number	Half reaction		$\Delta G^0(W)^*$ kJ per electron equivalent
	Reactions for bacterial cell synthesis (R_c)		
	Ammonia as nitrogen source:		
1.	$\frac{1}{5}CO_2 + \frac{1}{20}HCO_3^- + \frac{1}{20}NH_4^+ + H^+ + e^-$	$= \frac{1}{20}C_5H_7O_2N + \frac{9}{20}H_2O$	
	Nitrate as nitrogen source:		
2.	$\frac{5}{28}NO_3^- + \frac{5}{28}CO_2 + \frac{29}{28}H^+ + e^-$	$= \frac{1}{28}C_5H_7O_2N + \frac{11}{28}H_2O$	
	Reactions for electron acceptors (R_a)		
	Oxygen:		
3.	$\frac{1}{4}O_2 + H^+ + e^-$	$= \frac{1}{2}H_2O$	-78.14
	Nitrate:		
4.	$\frac{1}{5}NO_3^- + \frac{6}{5}H^+ + e^-$	$= \frac{1}{10}N_2 + \frac{3}{5}H_2O$	-71.67
	Sulfate:		
5.	$\frac{1}{8}SO_4^{2-} + \frac{19}{16}H^+ + e^-$	$= \frac{1}{16}H_2S + \frac{1}{16}HS^- + \frac{1}{2}H_2O$	21.27
	Carbon dioxide (methane fermentation):		
6.	$\frac{1}{8}CO_2 + H^+ + e^-$	$= \frac{1}{8}CH_4 + \frac{1}{4}H_2O$	24.11
	Reactions for electron donors (R_d)		
	Organic donors (heterotrophic reactions)		
	Domestic wastewater:		
7.	$\frac{9}{50}CO_2 + \frac{1}{50}NH_4^+ + \frac{1}{50}HCO_3^- + H^+ + e^-$	$= \frac{1}{50}C_{10}H_{19}O_3N + \frac{9}{25}H_2O$	31.80
	Protein (amino acids, proteins, nitrogenous organics):		
8.	$\frac{8}{33}CO_2 + \frac{2}{33}NH_4^+ + \frac{31}{33}H^+ + e^-$	$= \frac{1}{66}C_{16}H_{24}O_5N_4 + \frac{27}{66}H_2O$	32.22
	Carbohydrates (cellulose, starch, sugars):		
9.	$\frac{1}{4}CO_2 + H^+ + e^-$	$= \frac{1}{4}CH_2O + \frac{1}{4}H_2O$	41.84
	Grease (fats and oils):		
10.	$\frac{4}{23}CO_2 + H^+ + e^-$	$= \frac{1}{46}C_8H_{16}O + \frac{15}{46}H_2O$	27.61
	Acetate:		
11.	$\frac{1}{8}CO_2 + \frac{1}{8}HCO_3^- + H^+ + e^-$	$\Rightarrow \frac{1}{8}CH_3COO^- + \frac{3}{8}H_2O$	27.65
	Propionate:		
12.	$\frac{1}{7}CO_2 + \frac{1}{14}HCO_3^- + H^+ + e^-$	$= \frac{1}{14}CH_3CH_2COO^- + \frac{5}{14}H_2O$	27.88
	Benzoate:		
13.	$\frac{1}{5}CO_2 + \frac{1}{30}HCO_3^- + H^+ + e^-$	$= \frac{1}{30}C_6H_5COO^- + \frac{13}{30}H_2O$	28.84
	Ethanol:		
14.	$\frac{1}{6}CO_2 + H^+ + e^-$	$= \frac{1}{12}CH_3CH_2OH + \frac{1}{4}H_2O$	31.76
	Lactate:		
15.	$\frac{1}{6}CO_2 + \frac{1}{12}HCO_3^- + H^+ + e^-$	$= \frac{1}{12}CH_3CHOHCOO^- + \frac{1}{3}H_2O$	32.94
	Pyruvate:		
16.	$\frac{1}{5}CO_2 + \frac{1}{10}HCO_3^- + H^+ + e^-$	$= \frac{1}{10}CH_3COCOO^- + \frac{2}{5}H_2O$	35.75
	Methanol:		
17.	$\frac{1}{6}CO_2 + H^+ + e^-$	$= \frac{1}{6}CH_3OH + \frac{1}{6}H_2O$	37.51
	Inorganic donors (autotrophic reactions):		
18.	$Fe^{3+} + e^-$	$= Fe^{2+}$	-74.40
19.	$\frac{1}{2}NO_3^- + H^+ + e^-$	$= \frac{1}{2}NO_2^- + \frac{1}{2}H_2O$	-40.15
20.	$\frac{1}{8}NO_3^- + \frac{5}{4}H^+ + e^-$	$= \frac{1}{8}NH_4^+ + \frac{3}{8}H_2O$	-34.50
21.	$\frac{1}{6}NO_2^- + \frac{4}{3}H^+ + e^-$	$= \frac{1}{6}NH_4^+ + \frac{1}{3}H_2O$	-32.62

Energetics Cont.

- Energy Balance
    - Cell synthesis (R_c)
    - Energy (R_a)
    - Electron acceptor (R_d)

Reaction number	Half reaction		$\Delta G^0(W)^*$ kJ per electron equivalent
	Reactions for electron donors (R_d)		
	Inorganic donors (autotrophic reactions):		
22.	$\frac{1}{6}SO_4^{2-} + \frac{4}{3}H^+ + e^-$	$= \frac{1}{6}S + \frac{2}{3}H_2O$	19.48
23.	$\frac{1}{8}SO_4^{2-} + \frac{19}{16}H^+ + e^-$	$= \frac{1}{16}H_2S + \frac{1}{16}HS^- + \frac{1}{2}H_2O$	21.28
24.	$\frac{1}{4}SO_4^{2-} + \frac{5}{4}H^+ + e^-$	$= \frac{1}{8}S_2O_3^{2-} + \frac{5}{8}H_2O$	21.30
25.	$H^+ + e^-$	$= \frac{1}{2}H_2$	40.46
26.	$\frac{1}{2}SO_4^{2-} + H^+ + e^-$	$= \frac{1}{2}SO_3^{2-} + \frac{1}{2}H_2O$	44.33

*Reactants and products at unit activity except $[H^+] = 10^{-7}$. *Note:* 1 kcal $\sim$ 4.184 kJ.

$$R = f_s R_c + f_e R_a - R_d$$

From: Sawyer, McCarty & Parkin, 1994;
also: Sawyer & McCarty, 1978

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f-values and Yield

- Portions of electron donor used for:
    - Synthesis (f_s)
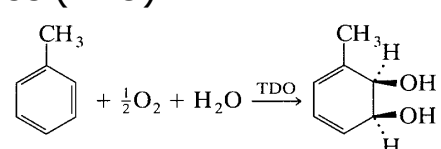   - Energy (f_e)
- Values are for rapidly growing cells

TABLE 6-5
Typical values for $f_{s(max)}$ for bacterial reactions

Electron donor	Electron acceptor	$f_{s(max)}$
Heterotrophic reactions		
Carbohydrate	O_2	0.72
Carbohydrate	NO_3^-	0.60
Carbohydrate	SO_4^{2-}	0.30
Carbohydrate	CO_2	0.28
Protein	O_2	0.64
Protein	CO_2	0.08
Fatty acid	O_2	0.59
Fatty acid	SO_4^{2-}	0.06
Fatty acid	CO_2	0.05
Methanol	NO_3^-	0.36
Methanol	CO_2	0.15
Autotrophic reactions		
S	O_2	0.21
$S_2O_3^{2-}$	O_2	0.21
$S_2O_3^{2-}$	NO_3^-	0.20
NH_4^+	O_2	0.10
H_2	O_2	0.24
H_2	CO_2	0.04
Fe^{2+}	O_2	0.07

From: Sawyer, McCarty & Parkin, 1994;
also: Sawyer & McCarty, 1978
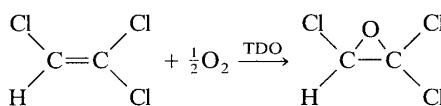
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Novel Biotransformations

- **Oxidation**
  - Toluene dioxygenase (TDO)

$$\text{Toluene} + \tfrac{1}{2}O_2 + H_2O \xrightarrow{\text{TDO}} \text{cis-dihydrodiol}$$

This enzyme will also oxidize TCE to its epoxide:

$$\text{TCE} + \tfrac{1}{2}O_2 \xrightarrow{\text{TDO}} \text{epoxide}$$

From: Sawyer, McCarty & Parkin, 1994;
also: Sawyer & McCarty, 1978

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Overall Types

- Carbon Source
  - Heterotrophic
  - Autotrophic
- Energy Source
  - Chemosynthetic
  - Photosynthetic

Photoheterotrophs (rare) — **Purple and green non-sulfur bacteria**

Photoautotrophs (primary producers) — **Cyanobacteria, algae & Plants**

Chemoheterotrophs (organotrophs) — **Most bacteria, fungi, protozoa & animals**

Chemoautotrophs (lithotrophs) — **Nitrifying, hydrogen , iron and sulfur bacteria**

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Enzyme Chemistry

- Highly dependent on:
  - Temperature
  - pH

From: Sawyer, McCarty & Parkin, 1994;
also: Sawyer & McCarty, 1978

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Enzymatic Reactions

- Many ways of illustrating the s
  - Substrate(s) bond to active site
  - Product(s) form via transition st
  - Product(s) are released

two substrate molecules

substrates contacting active site of enzyme

active site

substrates briefly bind tightly to enzyme active site

product molecule

enzyme unchanged by the reaction

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(a) Enzyme + Substrate
(b) Enzyme – substrate complex
(c) Transition state
(d) Enzyme – product complex
(e) Enzyme + Product

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Basic Enzyme Kinetics

Note that some references use k_2 for k_{-1}, and k_3 for k_2

- Irreversible

$$E + S \underset{k_{-1}}{\overset{k_1}{\rightleftarrows}} ES \overset{k_2}{\rightarrow} E + P$$

  - Single intermediate
    - The overall rate is determined by the RLS, k_2

$$r \equiv -\frac{d[S]}{dt} = \frac{d[P]}{dt} = k_2[ES]$$

    - But we don't know [ES], so we can get it by the SS mass balance

$$\frac{d[ES]}{dt} = 0 = k_1[E][S] - k_{-1}[ES] - k_2[ES]$$

    - Again, we only know $[E_o]$ or $[E_{tot}]$, not free [E], so:

$$0 = k_1([E_o] - [ES])[S] - k_{-1}[ES] - k_2[ES]$$

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Reactants, products and Intermediates

- Simple Progression of components for simple single intermediate enzyme reaction
  - Shaded block shows steady state intermediates
  - Assumes $[S] >> [E]_t$
  - From Segel, 1975; Enzyme Kinetics

$[S_0]$

Concentration

$[S]$ $[P]$

$[E]_T = [E] + [ES]$

$\frac{d[ES]}{dt} \approx 0$

$[E]_T$ $[ES]$

$[E]$

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Basic Enzyme Kinetics II

- And solving for [ES],

$$k_1[ES][S] + k_{-1}[ES] + k_2[ES] = k_1[E_o][S]$$

$$[ES] = \frac{k_1[E_o][S]}{k_1[S] + k_{-1} + k_2}$$

$$[ES] = \frac{[E_o][S]}{[S] + \frac{k_{-1}+k_2}{k_1}}$$

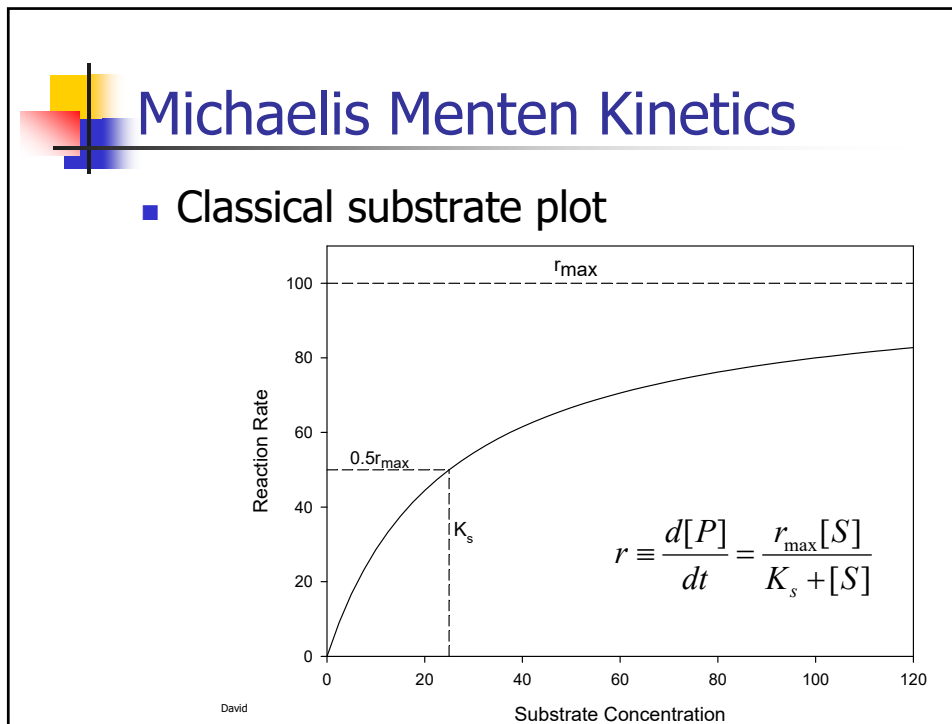David Reckhow   CEE 370 L#13   25

Michaelis-Menten

- **Irreversible**

$$E + S \underset{k_{-1}}{\overset{k_1}{\rightleftharpoons}} ES \overset{k_2}{\rightarrow} E + P$$

  - **Single intermediate**

$$r \equiv \frac{d[P]}{dt} = k_2[ES]$$

$$[ES] = \frac{[E_o][S]}{[S] + \frac{k_{-1}+k_2}{k_1}}$$

$$r \equiv \frac{d[P]}{dt} = \frac{k_2[E_o][S]}{\frac{k_{-1}+k_2}{k_1} + [S]} = \frac{r_{max}[S]}{K_s + [S]}$$

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Michaelis Menten Kinetics

- ## Classical substrate plot

$$r \equiv \frac{d[P]}{dt} = \frac{r_{max}[S]}{K_s + [S]}$$

The plot shows Reaction Rate (y-axis, 0 to 100) versus Substrate Concentration (x-axis, 0 to 120). The curve rises and approaches r_{max} (100). Labels: r_{max}, $0.5r_{max}$, K_s.

David

Maud Menten

Maud Menten

Maud Leonora Menten (March 20, 1879 – July 17, 1960)

- One of the first women to receive an advanced medical degree in Canada
- Completed some of the earliest research in treating cancer with radiation
- Completed early research on the benefit of vaccines on treating infectious disease in animals
- Published 100s of research papers
- Was among the first female faculty at Pitt

Menten as a petite dynamo of a woman who wore "Paris hats, blue dresses with stained-glass hues, and Buster Brown shoes."

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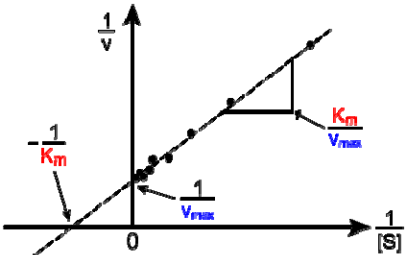
Substrate and growth

- If we consider Y

$$r \equiv \frac{d[P]}{dt} = -\frac{d[S]}{dt} = \frac{1}{Y}\frac{dX}{dt}$$

- We can define a microorganism-specific substrate utilization rate, U

$$U \equiv \frac{r}{X} = \frac{dX}{dt}\bigg/ YX \equiv \frac{\mu}{Y}$$

- And the maximum rates are then

$$U_{max} \equiv k \equiv \frac{\mu_{max}}{Y}$$

$$U \equiv \frac{1}{X}\frac{d[S]}{dt} = \frac{k[S]}{K_s + [S]}$$
and
$$\mu \equiv \frac{1}{X}\frac{d[X]}{dt} = \frac{\mu_{max}[S]}{K_s + [S]}$$
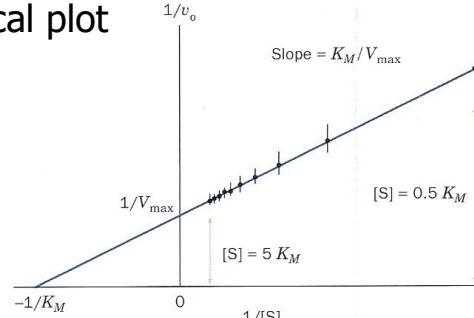
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Linearizations

- ### Lineweaver-Burke
  - Double reciprocal plot

Wikipedia version

Voet & Voet version

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- **To next lecture**

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